



**FLARE – OSBL PACKAGE SYSTEM ON LSTK BASIS AT
TALCHER FERTILIZERS LIMITED**
NIT NO : PNMM/PC-183/E- 4013/NCB, Dated-10.03.2022



Date 02.05.2022

Amendment –III

NIT NO.: PNMM/PC-183/E- 4013/NCB Dated-10.03.2022

Sub.: Flare – OSBL Package System ON LSTK basis at Talcher Fertilizers Limited.

This is for information of Bidders that **Amendment-III** date **02.05.2022** is being issued and shall be read in conjunction with the original Tender document issued on 10.03.2022 and all its subsequent amendments.

For & on behalf of
Talcher Fertilizers Limited (TFL)

P. R. Sahu
Addl. G.M (M.M)



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Sl. No.	Reference of Bidding Document				Existing Clause	Amendment Type	Amended Clause
	Part / Sec	Page No.	Clause No	Subject / Heading		M/D/A	
TECHNICAL							
1.0	VI	339 of 1215	Table-1	HP flare gas from Ammonia-Urea plant	Composition % (mole%) Typical (case 1.1): H2: 74.76(min), N2:24.94(min), Hg: 1ppmv (max), Ar: 30ppmv(max), CO + CO2+ other Oxygen bearing components: 5 ppmv (Max.) OR Typical(case 1.3): H2: 0.04, N2: 0.02, Ar: 0.01, NH3:99.93	M	Composition % (mole%) Typical (case 1.1): H2: 74.76(min), N2:24.94(min), Hg: 1ppmv (max), Ar: 30ppmv(max), CO + CO2+ other Oxygen bearing components: 5 ppmv (Max.) OR Typical(case 1.3): H2: 0.04, N2: 0.02, Ar: 0.01, NH3:99.93 Typical(case 1.1+1.3): H2: 49.95, N2: 16.67, Ar: 0.01, NH3:33.39



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2.0	VI	347 of 1215	Table-5	Ammonia flare gas header flow, kg/hr	<table border="1"> <tr> <td>3</td> <td>Ammonia flare gas from CGP</td> <td>CGP</td> <td>Ammonia flare gas header</td> <td>29073+101703=130776</td> <td>Cooling water failure & blocked outlet</td> <td rowspan="2">flaring</td> </tr> <tr> <td>4</td> <td>Ammonia flare gas from A & U</td> <td>A & U</td> <td></td> <td>266200</td> <td>Blocked outlet</td> <td>Ammonia flare</td> </tr> </table>	3	Ammonia flare gas from CGP	CGP	Ammonia flare gas header	29073+101703=130776	Cooling water failure & blocked outlet	flaring	4	Ammonia flare gas from A & U	A & U		266200	Blocked outlet	Ammonia flare	M	<p>Ammonia flare gas from CGP =29073 kg/hr Ammonia flare gas from A & U= 266200 kg/hr Total relief load for worst case scenario will be 266200+29073= 295273 kg/hr As relief from both sources may occur simultaneously.</p>
3	Ammonia flare gas from CGP	CGP	Ammonia flare gas header	29073+101703=130776	Cooling water failure & blocked outlet	flaring															
4	Ammonia flare gas from A & U	A & U		266200	Blocked outlet		Ammonia flare														
3.0	VI	345 & 346 of 1215	Table-4	Pressure at vendor's B/L for followings flare headers: a) Ammonia flare header b) Dry Seal flare header coming	a) 1.16 bar b) 1.01 bar	M	Pressure at vendor's B/L for followings flare headers have been revised to: a) 1.036 bar b) 1.017 bar														



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				from coal gasification (CGP) c) Dry Seal flare header coming from Ammonia & Urea (A & U)	c) 1.01 bar		c) 1.018 bar
4.0	VI	-	-	Simultaneous flaring case for calculation of flare radiation intensity.	-	A	Regarding flare radiation intensity calculation, only HP Gas Flare max. load flaring needs to be considered. Simultaneous flaring for different flare stacks (if any) can be covered by HP Gas Flare max. load flaring
5.0	VI	-	-	Minimum height of flare stack for the tendering purpose.	-	A	Height of flare stack should not be less than 50 m (considered based on the preliminary dispersion analysis).



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							However, actual flare height shall be calculated by bidder based on the actual Dispersion analysis, radiation intensity and simultaneous flaring, if any.

M: MODIFICATION, A: ADDITION, D: DELETION

Note: - The clauses in Amendment shall take precedence/superseded over all other pre bid replies against the respective clause.